## Evidences of the origin of  $N_2O$  in the high-temperature  $NH_3$  oxidation **over Pt–Rh gauze**

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**Transient isotopic experiments reveal that the mechanism of N2O formation in the high-temperature NH3 oxidation over Pt– Rh gauze involves the reaction of adsorbed ammonia intermediate species (NH***x***) and NO.**

Ammonia is oxidized over Pt–Rh alloy gauzes at 1073–1223 K to form NO as the first step in the industrial production of nitric acid, a process that has been in large-scale for over 80 years. The reaction typically yields 95–97% of NO and only 3–5% of by-products  $(N_2O)$ and  $N_2$ ).<sup>1</sup> Academic interest in the reaction lies in the challenge of elucidating details of the reaction mechanism and kinetics. However, despite numerous studies, there is still much uncertainty, particularly concerning the origin(s) of the reaction products.2 Surface science techniques in ultra-high vacuum (UHV) and in general low-pressure studies provided new insights into elementary reaction steps of ammonia oxidation leading to NO and  $N_2$  over Pt single crystals.3–9 However the robustness of this approach for achieving an accurate mechanistic description of the overall process is questionable, since  $N_2O$  was never detected as a product in UHV studies with model surfaces and thus its formation was not discussed. Accordingly, the reaction has been considered as biphasic in mechanistic terms,<sup>9</sup> yielding NO and  $N_2$ . This result has remained a puzzle for scientists in academic and industrial environments, since  $N_2O$  is formed in  $NH_3$  burners. In fact, nitric acid production is the largest single source of  $N_2O$  in the chemical industry (400 kton per year). Due to the environmental impact of N2O, producers have come under pressure to develop and implement abatement technology.2 Therefore understanding of the origin of  $N_2O$  is of great fundamental and practical relevance.

Herein, for the first time, we provide experimental evidences on the mechanism of  $N_2O$  formation in the high-temperature  $NH<sub>3</sub>$ oxidation over a commercial Pt–Rh alloy gauze. To this end, the Temporal Analysis of Products (TAP),10 a transient pulse technique, has been applied. A 28 mm2 piece of Pt–Rh gauze catalyst (95%Pt–5%Rh, K. A. Rasmussen, 1024 mesh per cm2 and wire diameter of  $76 \mu m$ ) was placed between two layers of quartz-sand in the isothermal zone of the TAP reactor (quartz, 6 mm i.d.). Prior to the experiments, the sample was pretreated in pure  $O_2$  at 1273 K and ambient pressure for 2 h. Then the catalyst was exposed to vacuum ( $ca$ . 10<sup>-5</sup> Pa) and transient experiments with <sup>15</sup>NH<sub>3</sub>, O<sub>2</sub>, and NO were carried out. Pulses containing a small amount of reactants diluted by an inert gas ( $\sim 10^{16}$  molecules per pulse,  $\lt 50$ nmol of reactant) were independently dosed in the reactor *via* two high-speed valves. The conversion of ammonia upon reaction with O2 or NO was studied at 973–1073 K using sequential pulse experiments, *i.e.* applying a certain time delay  $(\Delta t)$  between the two pulses. During pulsing, the peak pressure inside the TAP reactor was below 200 Pa. Isotopically labelled 15NH3 and 15NO were used in sequential pulsing with 14NO and 14NH3, respectively, in order to discriminate between  $N_2O$  and  $CO_2$  in mass spectrometry analysis. It is well known that the surface of commercial Pt-gauzes is covered by substantial amounts of carbon.11 Carbon deposits are oxidized to  $CO<sub>2</sub>$  during  $O<sub>2</sub>$  pulsing in the TAP reactor at 1023 K (even after pretreatment in pure  $O_2$  at 1273 K).

The normalised transient responses of selected reactants and products during sequential pulsing of <sup>16</sup>O<sub>2</sub>–<sup>15</sup>NH<sub>3</sub> and <sup>15</sup>NH<sub>3</sub>–<br><sup>14</sup>NO at  $\Delta t = 0.1$  s are shown in Figs. 1 and 2, respectively. For the sake of conciseness, we concentrate here on aspects relevant to  $N_2O$  formation. As shown in Fig. 1, the concentration of oxygen dramatically decreases at the time of the ammonia pulse at 0.1 s. The strong decrease of the O<sub>2</sub> signal reveals that adsorbed oxygen species formed during the O<sub>2</sub> pulse react with <sup>15</sup>NH<sub>3</sub> yielding <sup>15</sup>NO,  $15N_2$ ,  $15N_2O$ ,  $H_2$ , and  $H_2O$ . The shape of the NO and N<sub>2</sub>O responses is very narrow, and strongly differs from that of  $N_2$ , which is broader and shifted to longer times. The amount of  $N_2O$  formed decreased upon increasing temperature in the range of 973–1073 K (not shown), in good agreement with steady-state results at industrial conditions.<sup>2</sup> Surprisingly  $N_2O$  was not detected at time delays between oxygen and ammonia pulses  $> 0.1$  s, while the profiles of the other products were very similar (discussed later). *A priori*, from this result, one may conceive  $N_2O$  as a primary product of ammonia oxidation, *i.e.* originating from the direct reaction between  $NH_3$  and  $O_2$ . This pathway has been concluded for NO formation.3–9 For nitrous oxide, this hypothesis can be overruled by analysing the transient responses of  $N_2O$  during sequential pulsing of <sup>15</sup>NH<sub>3</sub> and <sup>14</sup>NO. In these experiments, N<sub>2</sub>O was observed at the time of the NO pulse (Fig. 2). The main N<sub>2</sub>O isotope produced was  $15N14NO$  (Fig. 3), which results from the N-pairing reaction



**Fig. 1** Transient responses during sequential pulsing of  $^{16}O_2$  and  $^{15}NH_3$  ( $\Delta t$  $= 0.1$  s) over Pt–Rh gauze at 1023 K. Pulse size of <sup>16</sup>O<sub>2</sub> and <sup>15</sup>NH<sub>3</sub>: 1.6·10<sup>16</sup> and 2.4·1016 molecules, respectively.



**Fig. 2** Transient responses during sequential pulsing of <sup>15</sup>NH<sub>3</sub> and <sup>14</sup>NO ( $\Delta t$ 0.1 s) over Pt–Rh gauze at 1023 K. Pulse size of  $15NH_3$  and  $14NO$ : 2.2·1016 and 3.0·1016 molecules, respectively.



**Fig. 3** Transient responses of 15N14NO and 15N15NO during sequential pulsing of <sup>15</sup>NH<sub>3</sub> and <sup>14</sup>NO ( $\Delta t = 0.1$  s) over Pt–Rh gauze at 1023 K. Pulse sizes as in caption of Fig. 2.

between  $15NH_3$  and  $14NO$ . The same result was obtained when  $14NH_3$  and  $15NO$  were sequentially pulsed.  $15N15NO$  is formed in much smaller amounts and stems from the reaction between  $15NH_3$ in the first pulse and 15NO eventually formed in the pulse of 14NO (see Fig. 2). <sup>15</sup>NO is produced at the time of the  $15\text{NH}_3$  pulse and rapidly reacts with remaining ammonia species, producing the limited amount of <sup>15</sup>N<sup>15</sup>NO observed. N<sub>2</sub>O formation from <sup>14</sup>NO would yield 14N14NO, but this mass cannot be detached from that of  $CO<sub>2</sub>$  in mass spectrometry. The irrelevance of this route for  $N<sub>2</sub>O$ formation was confirmed by performing single pulse experiments with 15NO at 1023 K, yielding only nitrogen as 15N15N. The implication of the Pt–Rh gauze in originating  $N_2O$  was further substantiated by performing simultaneous pulsing ( $\Delta t = 0$  s) of  $15NH_3$  and  $14NO$  at 1073 K in the TAP reactor filled with quartz sand. In this experiment, no  $N_2O$  was observed, so other potential contributions towards  $N_2O$  production, like homogeneous or heterogeneous processes on the reactor wall can be categorically excluded. Concluding,  $N_2O$  formation during the high-temperature ammonia oxidation over Pt–Rh alloy catalyst is mainly a product of the secondary reaction between ammonia and nitric oxide.

The heterogeneous nature of the reaction steps leading to  $N<sub>2</sub>O$ can be elegantly demonstrated by comparing the formation of  $15N14NO$  at different time delays between the  $15NH_3$  and  $14NO$ pulses. Fig. 4 shows a decreased formation of  $N_2O$  (at the time of the NO pulse) upon increasing the time delay between  $15NH_3$  and NO. Particularly significant is the decrease observed between 0.1 and 1 s. This result indicates the preferential  $N_2O$  formation over catalyst surface covered by adsorbed NH*<sup>x</sup>* species. At this stage, the influence of the oxygen species formed during the Pt–Rh gauze pretreatment in  $O_2$  (see Experimental) in N<sub>2</sub>O formation cannot be completely ascertained. What is clear is that adsorbed O-species are



**Fig. 4** Transient responses of 15N14NO during sequential pulsing of 15NH3 and <sup>14</sup>NO over Pt–Rh gauze at 1023 K at different time delays ( $\Delta t$ , in seconds). Pulse sizes as in caption of Fig. 2.

essential to activate ammonia by oxidative dehydrogenation, leading to reactive NH*<sup>x</sup>* fragments on the catalyst surface.8,9,12 This can also be concluded from the strong decrease of the  $O<sub>2</sub>$  signal at the time of the 15NH3 pulse in Fig. 1. The structure of the preferred NH*<sup>x</sup>* intermediate has been subject of controversy and remains unsolved. Both  $NH_{ads}$  and  $NH_{2,ads}$  species were found as intermediates in the ammonia oxidation reaction on the Pt(111) and Pt(100) surfaces.8,9,13

The isotopic TAP technique applied here has proven a unique experimental approach for deriving mechanistic insights into  $N_2O$ formation during the high-temperature ammonia oxidation, a highly exothermic reaction. The small size of the pulses, in the nmol range, enables an excellent control of temperature (estimated within 2 K at 1073 K). Operation under these conditions minimizes the presence of heat and mass transport limitations and prevents typical phenomena like ignition, extinction, hysteresis, and oscillations, which are extremely problematic in kinetic investigations with steady-state flow techniques.<sup>14,15</sup> Compared to UHV techniques, the TAP approach presents two advantages: it uses a real catalyst specimen instead of a model surface and much higher peak pressures can be achieved. The 'invisibility' of  $N_2O$  in previous UHV studies might be related to the fact that the concentration of  $N<sub>2</sub>O$  is below the detection limit of the analytical unit, as a consequence of the extremely low reactant peak pressures (typically  $10^{-5}$ – $10^{-7}$  Pa), which are apparently suitable for a proper analysis of NO and  $N_2$  but insufficient for  $N_2O$ . This can be related to the kinetics of products formation and its dependence with respect to the partial pressures of NH<sub>3</sub> and NO and requires a more detailed assessment.

The above evidence enables us to conclude that  $N_2O$  originates from the pairing of adsorbed ammonia intermediate species and nitric oxide. This result contributes to unravelling an important mechanistic feature of a classical reaction in one of the most traditional processes in modern chemical industry. The reaction pathway leading to  $N_2O$  is detrimental from two points of view, since it involves the loss of reactant (NH3) and desired product (NO). The origin of  $N_2O$  should be obviously situated in a region of the catalytic burner where NO is formed and some  $NH<sub>3</sub>$  remains unconverted, *i.e.* in the very first gauzes of the pack. This valuable information establishes the essential basis to design strategies for preventing or minimizing this undesired by-product in nitric acid production.

## **Notes and references**

- 1 E. Wagner and T. Fetzer, in *Handbook of Heterogeneous Catalysis*, **Vol. 4** , Eds.: G. Ertl, H. Knözinger and J. Weitkamp, VCH, Weinheim, 1997, pp. 1748–1761.
- 2 J. Pérez-Ramírez, F. Kapteijn, K. Schöffel and J. A. Moulijn, *Appl. Catal. B., Environ.*, 2003, **44**, 117 and references therein.
- 3 Ya. M. Fogel, B. T. Nadykto, V. F. Rybalko, V. I. Shvachko and I. E. Korobchanskaya, *Kinet. Catal.*, 1964, **5**, 431.
- 4 J. L. Gland and G. C. Woodward, *J. Catal.*, 1980, **61**, 543.
- 5 C. W. Nutt and S. Kapur, *Nature*, 1968, **220**, 697.
- 6 M. Asscher, W. L. Guthrie, T. H. Lin and G. A. Somorjai, *J. Phys. Chem.*, 1984, **88**, 3233.
- 7 S. H. Oh, H. Fisher, J. E. Carpenter and D. W. J. Goodman, *J. Catal.*, 1985, **100**, 360.
- 8 W. D. Mieher and W. Ho, *Surf. Sci.*, 1995, **322**, 151.
- 9 J. M. Bradley, A. Hopkinson and D. A. King, *J. Phys. Chem.*, 1995, **99**, 17032.
- 10 J. T. Gleaves, G. S. Yablonskii, P. Phanawadee and Y. Schuurman, *Appl. Catal. A: Gen.*, 1997, **160**, 55.
- 11 P. A. Kozub, G. I. Gryn and I. I. Goncharov, *Platinum Metals Rev.*, 2000, **44**, 74.
- 12 E. Kondratenko, V. Kondratenko, M. Baerns and J. Pérez-Ramírez, 2003, submitted.
- 13 A. C. M. van den Broek, A. C. M. van Grondelle and R. A. van Santen, *J. Catal.*, 1999, **185**, 297.
- 14 L. Andrussow, *Z. Angew. Chem.*, 1951, **63**, 350.
- 15 C. G. Takoudis and L. D. Schmidt, *J. Catal.*, 1983, **84**, 235.